















The agglomeration kernel is indeed an important parameter for modeling drum granulation processes. Not only the proper formulation of the size-independent part is needed, but also the dependency of agglomeration rate to particle size should be analyzed in order to obtain a proper model of the real plant.

## 6 Conclusions

In this paper, a comparative study on various model forms for representing a drum granulation process is given. Different granulation mechanisms are compared based on simulation results represented by particle size distributions and the  $d_{50}$  diameter (to reflect the average size of particles) at the influent and the effluent of the drum granulator. For the drum granulator under consideration, the simulation results lead to the following conclusions:

- Particle growth due layering has very small effect on the change of the particle sizes compared to particle binary agglomeration.
- Inclusion of the particle size dependency on the agglomeration kernel affects the mass distribution function, i.e., particles with a wider PSD and larger particles are produced compared to simulations with a constant agglomeration kernel.
- The combined process increases the growth of particles by  $\sim 7\%$  (with size-independent kernel) and by  $\sim 10\%$  (with size-dependent kernel) compared to a pure agglomeration process.

The choice of the agglomeration kernel directly affects the PSD of the particles. The size-independent part of the kernel should be calculated by taking into account the operational parameters of the actual drum granulator.

## 7 Acknowledgment

The economic support from The Research Council of Norway and Yara Technology Centre through project no. 269507/O20 'Exploiting multi-scale simulation and control in developing next generation high efficiency fertilizer technologies (HEFTY)' is gratefully acknowledged.

## References

J. Drechsler, M. Peglow, S. Heinrich, M. Ihlow, and L. Mörl. Investigating the dynamic behaviour of fluidized bed spray granulation processes applying numerical simulation tools. *Chemical Engineering Science*, 60(14):3817–3833, 2005.

A.M. Golovin. The solution of the coagulation equation for raindrops, taking condensation into account. *Soviet Physics-Doklady*, 8(2):191–193, 1963.

S. Heinrich, M. Peglow, M. Ihlow, and L. Mörl. Particle population modeling in fluidized bed-spray granulation - analysis of the steady state and unsteady behavior. *Powder Technology*, 130:154–161, 2003. doi:10.1016/S0032-5910(02)00259-0.

S.M. Iveson, J.D. Litster, K. Hapgood, and B.J. Ennis. Nucleation, growth and breakage phenomena in agitated wet granulation processes: a review. *Powder technology*, 117(1-2): 3–39, 2001.

PC Kapur. Kinetics of granulation by non-random coalescence mechanism. *Chemical Engineering Science*, 27(10):1863–1869, 1972.

P.C. Kapur and D.W. Fuerstenau. Coalescence model for granulation. *Industrial & Engineering Chemistry Process Design and Development*, 8(1):56–62, 1969.

B. Koren. A robust upwind discretization method for advection, diffusion and source terms. In C. B. Vreugdenhil and B. Koren, editors, *Numerical Methods for Advection-Diffusion Problems, Notes on Numerical Fluid Mechanics*, pages 117–138. 1993.

J. Kumar. *Numerical approximations of population balance equations in particulate systems*. PhD thesis, Otto-von-Guericke-Universität Magdeburg, Universitätsbibliothek, 2006.

J. Kumar, M. Peglow, G. Warnecke, S. Heinrich, and L. Mörl. Improved accuracy and convergence of discretized population balance for aggregation: The cell average technique. *Chemical Engineering Science*, 61(10):3327–3342, 2006.

J. Litster and B. Ennis. *The science and engineering of granulation processes*, volume 15. Springer Science & Business Media, 2004.

MATLAB. 2017a. The MathWorks, Inc., Natick, Massachusetts, United States., 2017.

L. Mörl. *Anwendungsmöglichkeiten und Berechnung von Wirbelschichtgranulationstrocknungsanlagen*. PhD thesis, Technische Hochschule Magdeburg, 1981.

L. Mörl, M. Mittelstrab, and J. Sachse. Zum kugelwachstum bei der wirbelschichttrocknung von suspensionen oder losungen. *Chemical Technology*, 29(10):540–541, 1977.

R. Radichkov, T. Müller, A. Kienle, S. Heinrich, M. Peglow, and L. Mörl. A numerical bifurcation analysis of continuous fluidized bed spray granulator with external product classification. *Chemical Engineering and Processing*, 45:826–837, 2006. doi:10.1016/j.cep.2006.02.003.

D. Ramkrishna. *Population balances: Theory and applications to particulate systems in engineering*. Academic press, 2000.

A.D. Randolph and M.A. Larson. Transient and steady state size distributions in continuous mixed suspension crystallizers. *AIChE Journal*, 8(5):639–645, 1962.

F.Y. Wang and I.T. Cameron. A multi-form modelling approach to the dynamics and control of drum granulation processes. *Powder Technology*, 179(1-2):2–11, 2007.

F.Y. Wang, X.Y. Ge, N. Balliu, and I.T. Cameron. Optimal control and operation of drum granulation processes. *Chemical Engineering Science*, 61(1):257–267, 2006.